

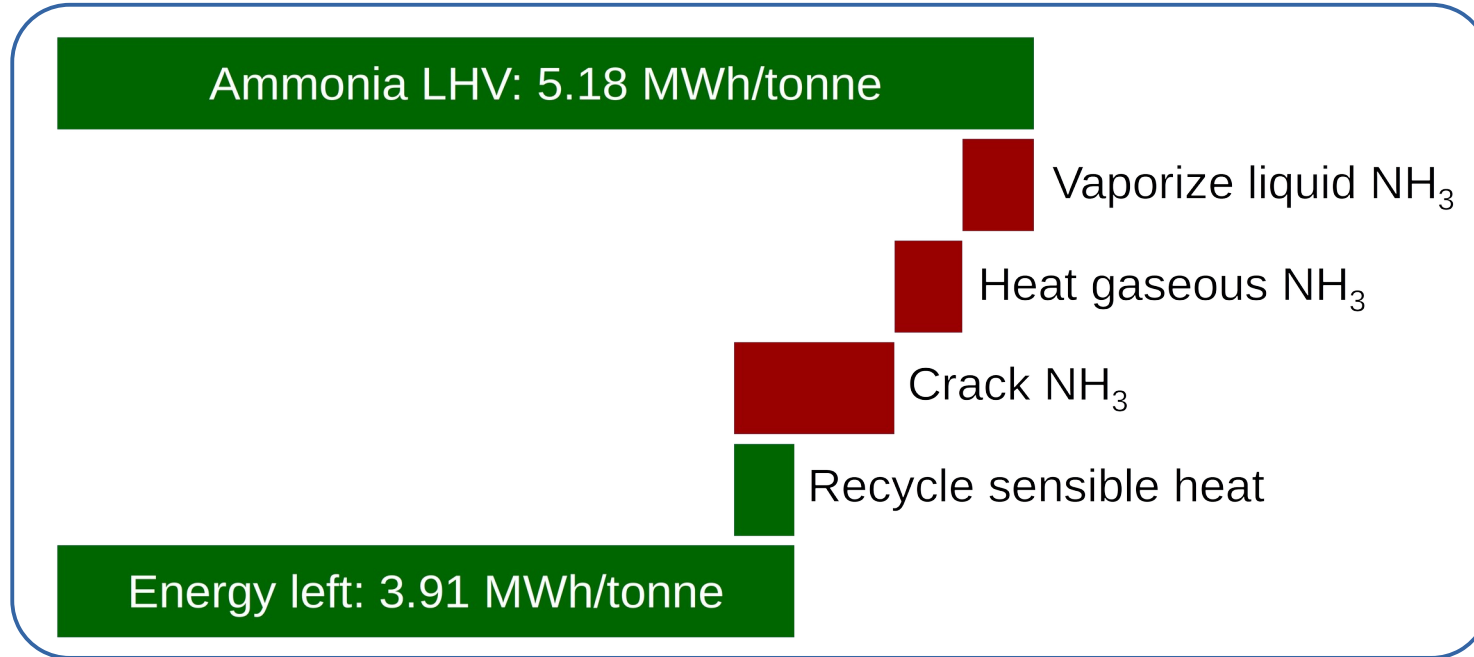


Cracking ammonia for $\text{NH}_3 + \text{H}_2$ blends or high purity H_2

17 November 2020

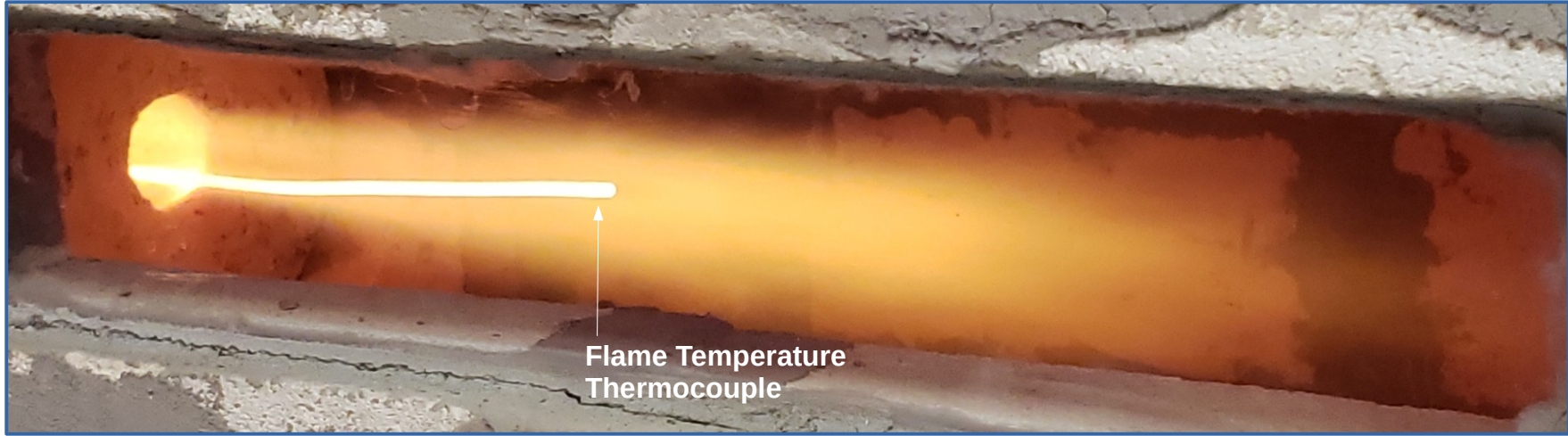
Joe Beach

Use ammonia as a direct fuel when possible



- Cracking consumes ~25% of stored energy *if done perfectly*
- Strong incentive to minimize cracking

Pure + cracked NH_3 burns like natural gas

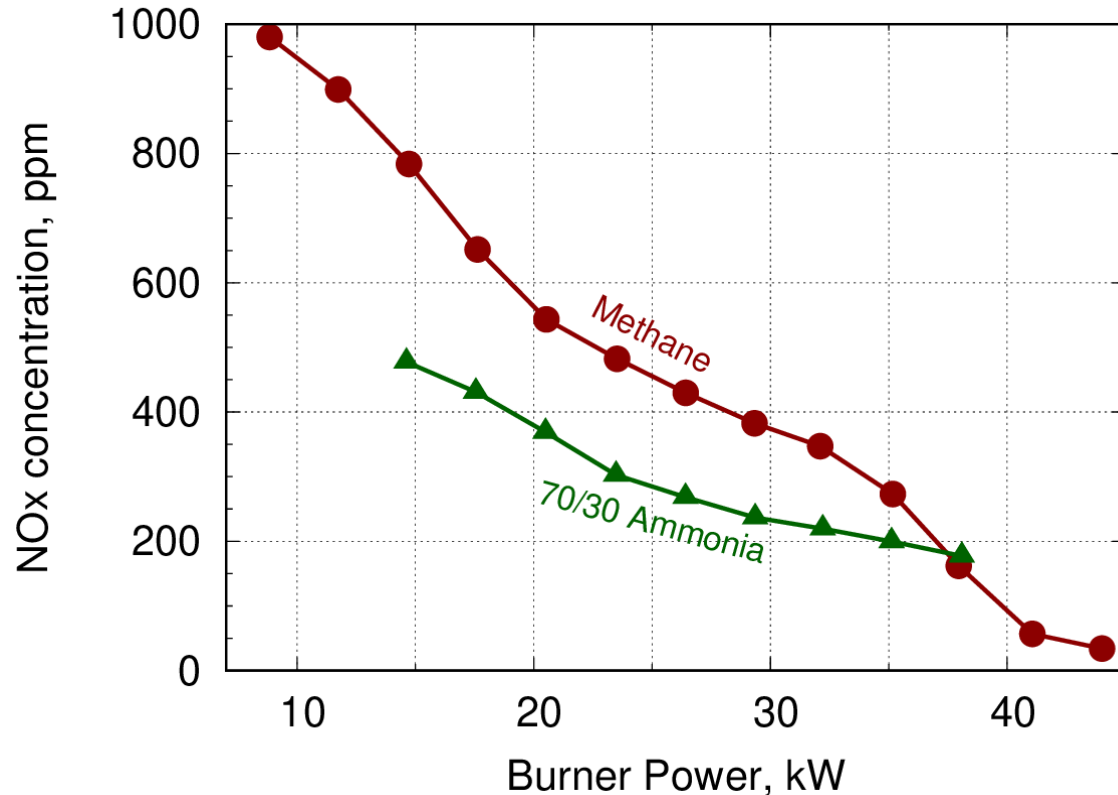


38kW burner flame, 70% mole fraction ammonia, 30% cracked ammonia (H_2 and N_2). Photo credit: Jenn Beach

- Commercial 44 kW / 150,000 BTU/h natural gas burner
- 70% NH_3 + 30% simulated cracked NH_3
- Stoichiometric fuel:air ratio

70+30 blend has reasonable NOx emissions

NOx emissions from 70/30 NH₃ or CH₄ in same burner



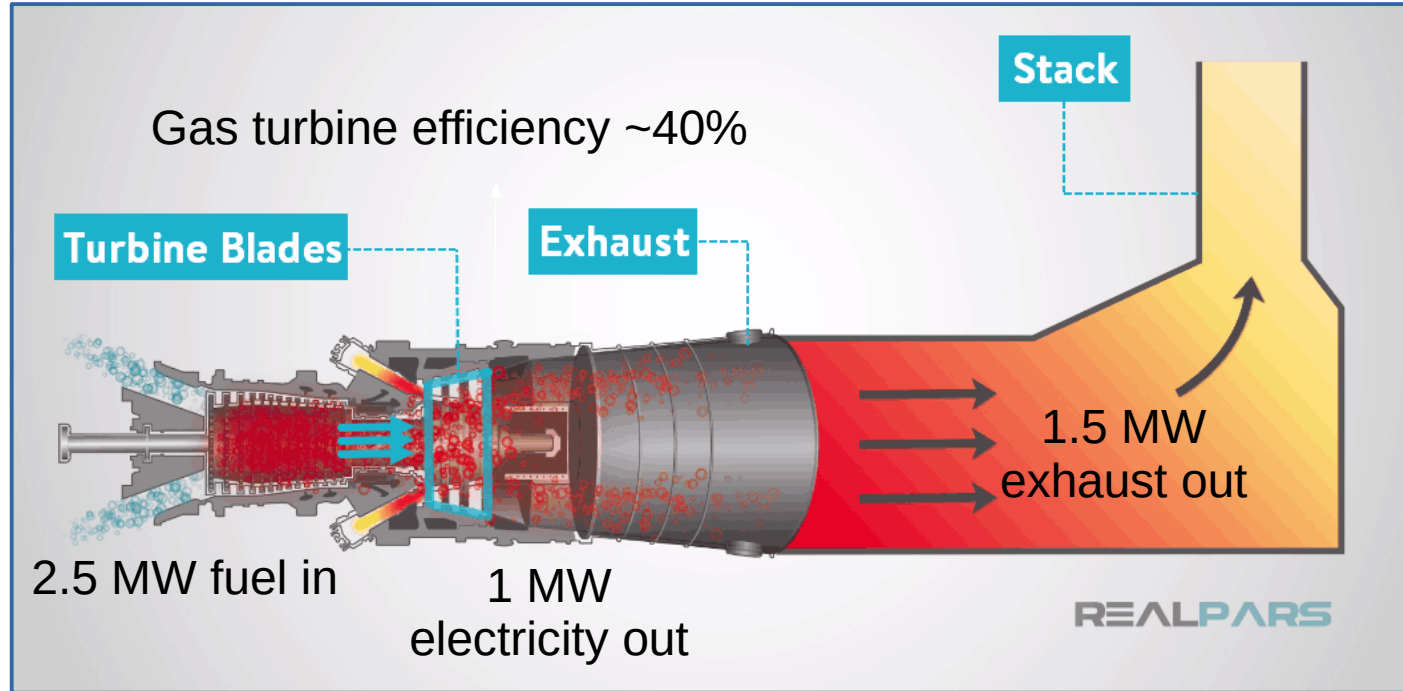
Methane fuel emissions

- NOx drops with burner power
- Sharp drop at 36-38 kW
- 50 ppm NOx at high power

Ammonia fuel emissions

- NOx drops with burner power
- NOx < 200 ppm at 38 kW
- Max power limited by air blower

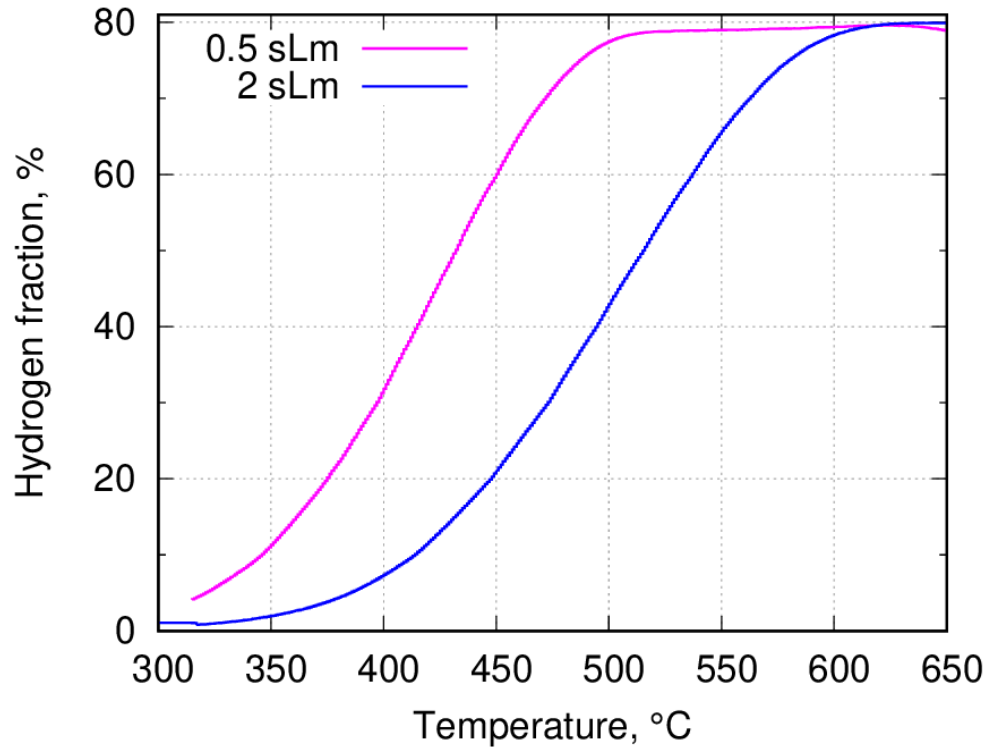
Gas turbines have waste heat opportunity



- 70/30 blend: 0.183 MW heat input for cracking
- Hot exhaust becomes useful heat for cracking

Cracking is compatible with exhaust heat

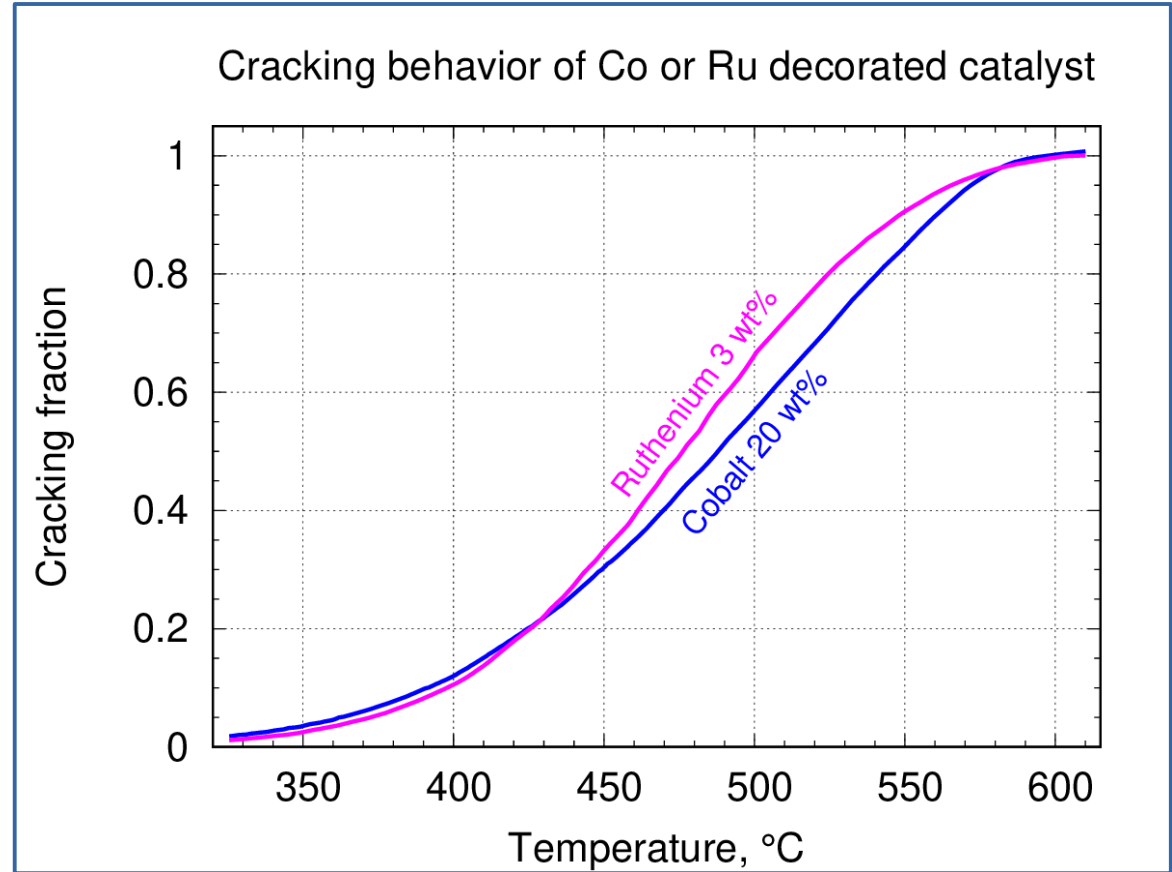
Ru-based monolith NH_3 cracking



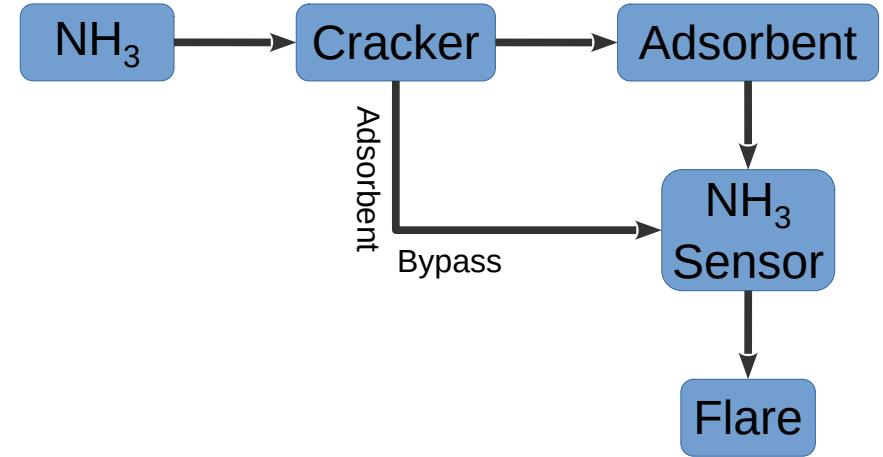
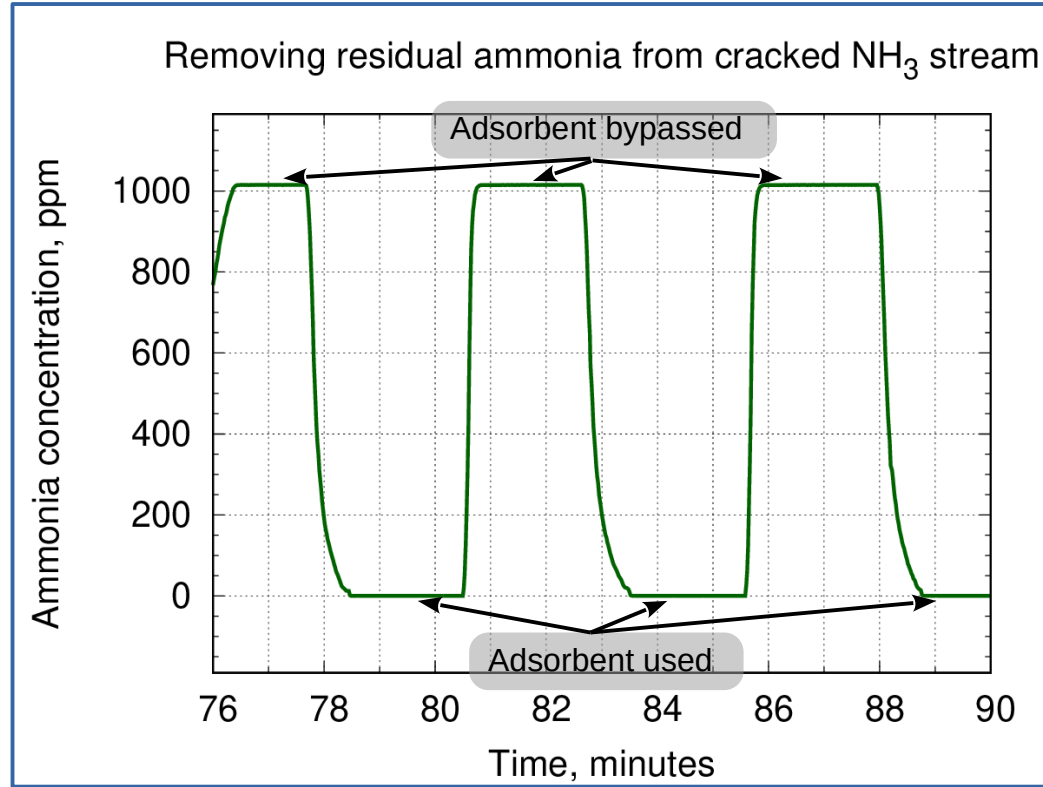
- Starfire Energy catalyst
- Bonded to metal monolith
- High catalyst utilization
- Scaling up process

Cobalt catalyst works also

- Both on B2CA support
- Both on metal monolith
- Both 1 sLm NH_3 flow
- Cobalt stable during 90 h continuous test



Residual NH_3 removal demonstrated



- 0-1000 ppm NH_3 detector
- “Full cracking” $\text{NH}_3 > 1000$ ppm
- Nominally 0 ppm residual NH_3
- Path to 99.999%, >700 bar H_2



Thank you.

I'm happy to answer questions
during the panel discussion

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